



Spherical montmorillonite-supported molybdenum disulfide nanosheets as a self-sedimentary catalyst for organic pollutants removal

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ABSTRACT

Water containing organic and carcinogenic pollutants has become a serious environmental problem, threatening the life of the aquatic ecosystem and human beings. Molybdenum disulfide (MoS₂), especially monolayered MoS₂ sheets, has been proven as an effective catalyst for degradation of organic contaminants due to its more exposed edges and active sites for electron transfer. However, monolayered MoS₂ nanosheets easily aggregate due to their high surface energy and strong π - π electron interaction, heavily affecting the catalytic performances. In addition, monolayered MoS₂ nanosheets with small tiny size are difficult to recover from the mixture, restricting the capacity of recyclability and further mass application. Herein, we solved these issues via supporting the small tiny MoS₂ nanosheets on spherical montmorillonite (SMT). The SMT can not only provide large pore volume and specific surface area for supporting abundant MoS₂ but also reduce the fouling and enhance the transport during the mass production process. The prepared microspheres exhibited a high catalytic activity towards organic pollutants including methylene blue (MB) and 4-nitrophenol (4-NP) in the presence of NaBH₄ due to the strong adsorption capacity of SMT and the large catalytic surface area for electron transfer. Furthermore, the micro-sized granular catalyst can be facile recovered and reused without any devices involved due to the excellent self-sedimentary capacity and large size. Moreover, the catalytic performance and the morphology were almost unaltered after recycling 20 times. Our straightforward strategy to solve the issues through porous micro-sized self-sedimentary SMT supporting tiny monolayered MoS₂ nanosheet with high catalytic activity facilitates the practical application of these kinds of catalyst towards the reduction of organic and carcinogenic pollutants.

1. Introduction

Most of the organic dyes and their intermediates are carcinogenic and easily soluble in water [1]. Very low concentration in water can alter the color, thus changing the refraction index of water, which is not only caused the visual pollution but also interfered with the absorb sunlight of aquatic life [2–5]. To solve this problem, a variety of approaches have been developed to remove these pollutants, including physical adsorption [6,7], chemical and biological methods [8]. Among them, chemical catalytic method has been proved as an effective

approach to fast degradation with low cost and easy operation [9–14]. Layered ultrathin two-dimensional (2D) nanomaterials have become one of the most promising catalytic materials due to their capacity of providing abundant active sites for catalysis [15,16]. As one of the typical 2D nanomaterials, molybdenum disulfide (MoS₂) nanosheets consist of covalently bonded S-Mo-S layers [17]. Compared with bulk MoS₂, mono- or few layered MoS₂ nanosheets provide abundant active sites for catalytic reduction of organic pollutants due to its under-coordinated sulfur atoms at the edges [18]. However, the nanosheets easily stack together due to van der Waals interaction during the

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catalytic process, thereby heavily decrease the number of active sites and catalytic activity. Previously, nanoparticles such as carbon nanotube [19], graphene [20,21], and TiO_2 [22] were used as the nano-supported substrate to disperse and anchor the MoS_2 nanosheets. These nano-sized substrates were well hybridized or wrapped by the MoS_2 nanosheets to obtain the stable carbon nanotube/ MoS_2 , graphene/ MoS_2 , and $\text{TiO}_2/\text{MoS}_2$ nanocomposites. Nevertheless, the application of these fabricated nanocomposites was still limited by the critical issues of recyclability due to their tiny nano size.

Montmorillonite (Mt) is a natural nanomaterial, has strong adsorption capacity and has been used as a good substrate for supporting MoS_2 [23–29]. For example, Peng et al. designed and successfully fabricated Mt/ MoS_2 catalyst with MoS_2 nanosheets intercalating in the interlayer of Mt [30] and MoS_2 nanosheets depositing on the surface of Mt [31]. Although the prepared Mt/ MoS_2 catalyst exhibited a good catalytic activity towards organic pollutant 4-nitrophenol (4-NP), their mass applications are still restricted by the problem of recyclability because the deposit rate of Mt based catalyst in the mixture is highly limited by the excellent hydrophilicity and swelling ability of Mt. Therefore, a great number of recovered devices are involved which heavily increases the cost of wastewater treatment.

Spray-drying is a proven technique in the industry to fabricate granulation with microsize to millimeter-size [32]. In our previous work, Mt were granulated to spherical micro-sized microsphere through this technology [33–35]. The stacked Mt forms a porous structure and provides abundant surface areas to support active sites. In addition, the granular treatment can obviously enhance the transport ability during the productive process, facilitating mass production of these kinds of catalysts [36]. Furthermore, the density of the prepared granular Mt microsphere is much higher than the mixture, which can be self-sedimentary and easy recovered from the bottom. In this work, we fabricated micro-sized spherical Mt (SMt) with large specific surface areas, followed by adhering to the tiny MoS_2 nanosheets on the surface of SMt through the polydopamine (PDA) coating [37]. PDA has been demonstrated the strong adhesion on various substrates [38]. The model organic pollutants, methylene blue (MB) and 4-nitrophenol (4-NP) were selected to evaluate the catalytic performances. Moreover, the recyclability was investigated. As we know, this is the first report of synthesized SMt/ MoS_2 for catalytic reduction of MB and 4-NP, successfully solving the engineering problem through a physical method.

2. Experimental

2.1. Chemicals

All chemicals and reagents were used as received without any further purification. They include dopamine hydrochloride (DA, Sigma Aldrich, $\geq 98.0\%$), monolayered molybdenum disulfide (MoS_2 , Sigma-Aldrich, $\geq 98.0\%$), montmorillonite (Mt, (Na, K, Ca) $_{0.33}(\text{Al}_{1.67}\text{Mg}_{0.33})\text{Si}_4\text{O}_{10}(\text{OH})_2 \cdot n\text{H}_2\text{O}$), Sinopharm Chemical Reagent Co. Ltd., China, $\geq 98.0\%$), methylene blue (MB, Tianjin Guangfu Reagent Co., China, $\geq 98.0\%$), 4-nitrophenol (4-NP, Tianjin Guangfu Reagent Co., China, $\geq 98.0\%$), sodium borohydride (NaBH_4 , Sinopharm Chemical Reagent Co. Ltd., China, $\geq 99.0\%$), and Tris-HCl buffer (Beijing Solarbio Science & Technology Co., Ltd, China).

2.2. Granulation of Mt and fabrication of spherical Mt supported MoS_2

Spray drying technology was applied to fabricate spherical Mt (SMt). First, 10.0 g Mt was mixed with 100 mL ethanol and sonicated for 4 h. Then the suspension was adding to the spray-dryer (YC-015, Shanghai Pilotech Instrument & Equipment Co. Ltd) using a peristaltic pump. The feed rate was set as 50 mL min^{-1} and the drying temperature was set as 110°C , respectively. Finally, the granular SMt with the mean size of about $20 \mu\text{m}$ was obtained. The prepared SMt was used as the substrate to support MoS_2 . Typically, 1.0 g DA and 20 mM

Tris-HCl buffer were added in 200 mL water to form the mixture. The pH was adjusted to 8.5 using 0.1 M of NaOH solution. After the color of the solution changed to dark yellow, 2.0 g SMt was added to form the suspension. Through 6 h shaking, the color of suspension changed to black and then filtered. The black product was fully washed by a 25% isopropyl alcohol-water solution and then dried in a vacuum oven at 60°C for 24 h to obtained the black microsphere. On the other hand, the monolayered MoS_2 nanosheets were mixed in aqueous solution with a concentration of 0.1 mg mL^{-1} , followed by ultrasound treatment for at least 4 h via a cell disruptor to get the dark black suspension. The dark black suspension was separated by the centrifugal separation at 12,000 rpm for 2 min. The faint yellow supernatant was extracted and mixed with the prepared black microsphere using a rotator for at least 6 h. After the filter separation, the microspheres were dried to obtain the final product.

2.3. Characterization

The Fourier transform infrared (FTIR) spectra of samples were obtained through a Perkin-Elmer 2000 Fourier transform infrared spectrometer with KBr pressed pellets. Scanning electron microscopy (SEM) was performed using a Jeol S4800 scanning electron microscope and an energy-dispersive detector. Transmission electron microscopy (TEM) and atomic force microscopy (AFM) were carried out using a JEM-2200 transmission electron microscope and Multi-Mode 8 atomic force microscope, respectively. X-ray diffraction (XRD) measurements were performed with Bruker D8-Advantage powder diffractometer using $\text{Cu K}\alpha$ radiation (40 kV, 110 mA). X-ray photoelectron spectroscopy (XPS) measurements were taken using Thermo EscaLab 250Xi spectrometer. Nitrogen adsorption measurements were carried out at 77 K using an ASAP2020 analyzer. The UV absorption spectra were measured using a PERSEE UT 1810 UV-vis spectrometer.

2.4. Adsorption experiment

10.0 mg samples were engaged in a 100 mL aqueous solution containing 100 mg L^{-1} MB and fully mixed. Then the UV-vis absorption spectra of organic pollutants at a certain interval were recorded. The removal percentages of organic pollutants are calculated following the equation (1) [6]:

$$R = \left(\frac{C_0 - C_t}{C_0} \right) \times 100\% \quad (1)$$

Where R is the removal percentage of organic dyes, the C_0 (mg L^{-1}) and C_t (mg L^{-1}) are the initial dye concentration and the concentration of reaction time, respectively.

The equilibrium concentration is calculated according to equation (2) [39]:

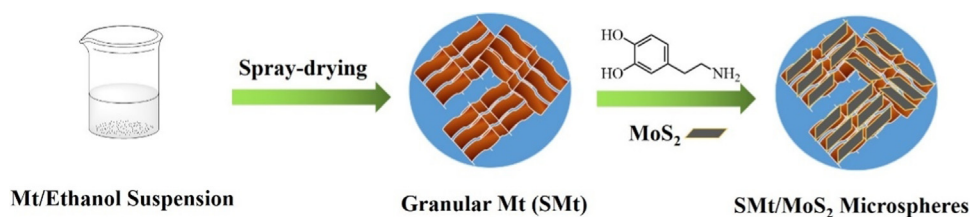
$$q_e = (C_0 - C_e)V/W \quad (2)$$

Where q_e is the amounts of organic pollutants adsorbed on the samples at equilibrium, C_0 (mg L^{-1}) and C_e (mg L^{-1}) are the initial and equilibrium concentrations of organic pollutants solution, respectively, V is the volume of the reaction solution (L) and W is the mass (g) of the samples.

The reduction efficiency of organic pollutants is calculated following the equation (3):

$$E = \left(\frac{C_0 - C_t}{C_0} \right) \times 100\% \quad (3)$$

Where E is the reduction efficiency of organic pollutants, the C_0 (mg L^{-1}) and C_t (mg L^{-1}) are the initial and equilibrium concentration of organic pollutants, respectively.



Scheme 1. The synthesized route for the fabrication of SMT/MoS₂ microsphere, including the first spray-drying and further fixed tiny MoS₂ nanosheets on the prepared SMt through dopamine chemistry method.

2.5. Catalytic reduction

The catalytic reduction of organic dyes was carried out to assess the catalytic activity and reusability of the prepared microsphere. The calibration curves of organic dyes and their intermediates are shown in Fig. S1. Typically, 10 mL organic dyes (250 mg L⁻¹) and 20 mg (200 mg L⁻¹) catalyst were mixed with 80 mL deionized water. After fully stirring, 10 mL NaBH₄ (0.5 M) aqueous solutions was added. As the color of organic dyes vanished, the prepared microsphere was easily separated from the mixture due to the self-sedimentary property. Then, the catalyst was further added to the new solution containing organic dyes and NaBH₄ to finish one cycle. All the processes were fully recorded by the UV-vis spectrometer.

3. Results and discussion

3.1. Synthesis and characterization of SMT/MoS₂ microspheres

Porous granular Mt substrates were first prepared through the spray-drying technology. As shown in Scheme 1, after fully sonicated with ethanol, the mixed suspension was granulated through a spray dryer. The granular Mt was modified by dopamine and a black coating was formed on the surface. The strong adhesion capacity of PDA coating could easily fix the tiny MoS₂ nanosheets and thus fabricated the SMT/MoS₂ microsphere.

The granulation process of Mt is not only enhanced the size of Mt but also improved the pore size and flowability of the prepared catalyst [36]. Therefore, the morphology was observed by the SEM, TEM, and AFM. As shown in Fig. 1a, the pristine Mt exhibits an amorphous morphology with the Mt sheets loose stacking (Fig. S2a). After the spray-drying process, the granular particle with a smooth surface and a mean diameter of about 20 μm were successfully fabricated (Fig. 1b). The PDA coated process has almost unaltered the morphology (Fig. 1c). However, the obviously rough surface could be observed after deposited MoS₂ nanosheets (Fig. 1d). Difference from the pristine Mt, a dense and porous morphology with Mt sheets tight stacking can be observed from Fig. S2b. As shown in the inset of Fig. 1d and Fig. S3, a thin ~4 nm layer was well deposited on the SMt. The small nanosheets were determined to be MoS₂, exhibiting strong Mo and S element peaks by EDX shown in Fig. S4. The crystal phases of MoS₂, SMt, and SMT/MoS₂ microsphere were analyzed by X-ray diffraction, and the data is exhibited in Fig. 2. The SMt with the crystallite size of 14.9 nm calculated from the (100) peak using Scherrer equation contained smectite (fcc, JCPDS card no. 13-0135) and quartz (fcc, JCPDS card no. 46-1045) [40]. The peaks at 2θ of 14.2°, 32.9°, 39.1°, 48.5°, and 58.3° appear, which can be assigned to the (002), (100), (103), (105), and (110) crystal faces of 2H-MoS₂ (fcc, JCPDS card no. 37-1492), confirming the successfully supported MoS₂ on the SMt (Fig. 2) [20,25]. The crystallite size of MoS₂ nanosheets was estimated from (002) peak as 7.7 nm, which is similar to the result of AFM (the thickness of the nanosheets is about 4 nm, Fig. 1e). The small-sized nanosheets can be easily supported on the micro-sized SMt substrates and provided abundant active sites for the reaction. For the SMT/MoS₂ microsphere, it exhibits the peaks of SMt and MoS₂, reflecting the good composition of SMT/MoS₂ microsphere. The crystallite size of SMT/MoS₂ microsphere was calculated as 14.5 nm, which is almost the same with the SMt,

demonstrating the higher content of SMt in the SMT/MoS₂ microsphere. XPS measurements were carried out to investigate the surface elemental composition and chemical status of the prepared microsphere. As shown in Fig. 1f, the peaks corresponding to C, O, Si, S, Al, and Mo can be observed, well consistent with the formation of SMT/MoS₂ microsphere. The atomic percentages of Mo and S elements on the surface of the microsphere were calculated as 0.11% and 0.17%, which is well agreeing with the theoretical values for MoS₂. As shown in Fig. S5, for the pristine MoS₂ nanosheets, the peaks of Mo 3d_{3/2}, Mo 3d_{5/2}, and S 2s are 233.1 eV, 229.7 eV, and 226.9 eV, respectively. The higher peak at 237.1 eV is assigned to the Mo 3d_{3/2} of MoO₃, which is derived from the adsorbed oxygen molecule [20]. For the samples of SMT/MoS₂ microsphere, no peak of MoO₃ can be observed (Inset of Fig. 1f), demonstrating the no effect of catalytic activity of SMT/MoS₂ microsphere. Furthermore, the peaks of Mo 3d are shifted to the higher energy value, reflecting the electronic interaction between MoS₂ and SMt. The enhanced interaction facilitates the improve the stability of microsphere, thereby maintaining the catalytic activities and benefiting the recovery and reuse. In addition, corresponding to the TEM image, the EDX mapping of Mo and S elements exhibit the same region, demonstrating the immobilization supporting of MoS₂ nanosheet in the fabricated microsphere (Fig. 3). Furthermore, the loading of Mo was quantified by ICP/MS to be 0.4 wt% upon dissolving SMT/MoS₂ microsphere in the strong acid, that is, the loading of MoS₂ was calculated to be 0.67 wt%. Considered the small tiny size MoS₂ uniformly dispersion on the SMt, the content of loading MoS₂ nanosheet can provide the abundant tiny active sites for catalytic reduction of organic pollutants.

3.2. Adsorption experiments

Through the granulation process, the Mt was stacked to the 2D microsphere, thus the changes of specific surface area and pore properties were measured by the N₂ adsorption. As shown in Fig. 4a and Table 1, compared with pristine Mt with a BET specific surface area of 8.2 m² g⁻¹ and a total pore volume of 0.1 cm³/g, the values of granular SMt greatly improved to 60.6 m²/g and 0.38 cm³/g, respectively, reflecting the well pore-making ability of spray-drying. Furthermore, the values were slightly decreased to 45.6 m²/g and 0.24 cm³/g after the surface coating process and further decreased to 31.3 m²/g and 0.20 cm³/g after the supporting process, which is still much higher than pristine Mt. The decreased values after the supporting process is mainly due to the weak N₂ adsorption capacity of MoS₂, as shown in Fig. 4a and Table 1. The large pore size will benefit the adsorption and catalytic reduction of organic dyes due to the opportunity for contacting with the catalyst and organic dyes. The adsorption towards organic dyes was monitored by UV-Vis absorption spectra and MB with the band of 665 nm was selected as a model here. Samples including pristine Mt, SMt, PDA-coated SMt, and SMT/MoS₂ exhibited similar adsorption with three stages, the first fast adsorption process, gradually increased stage, and the final equilibrium stage. Although all samples exhibited similar first fast adsorption behaviors, the gradual stage is quite different due to the differences of the intra-particle diffusion-rate controlling process. Compared with the pristine Mt, the intra-particle diffusion-rate of SMt, PDA-coated SMt, and SMT/MoS₂ is prolonged. The samples reach the equilibrium stage as the max

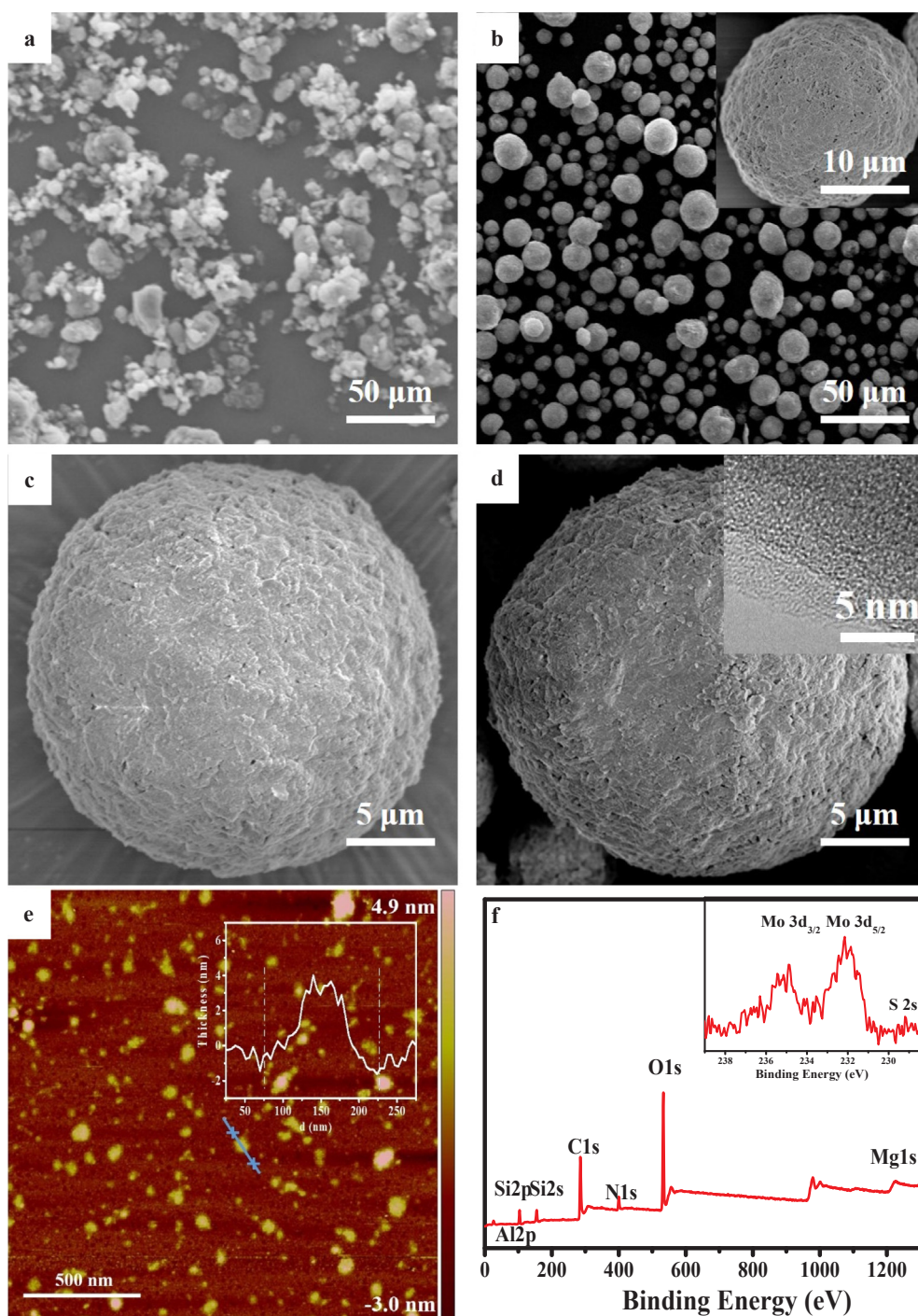


Fig. 1. SEM images of the Mt (a), SMT (b) with inset enlarging image, PDA@SMT (c) and SMT/MoS₂ (d) microspheres with inset high-resolution TEM spectra. AFM image with inset corresponding thickness of MoS₂ nanosheet (e). XPS spectra of SMT/MoS₂ with inset high-resolution XPS spectra of Mo 3d and S 2s regions (f).

adsorption is achieved (Fig. 4b). Among the samples, SMT exhibited the largest adsorption capacity of 992 mg g⁻¹, which is increased about 68.7% compared with pristine Mt. It can be attributed to the well granular process of Mt. SMT/MoS₂ slightly decreased the adsorption capacity to 870 mg g⁻¹, the value is much higher than other substrates reported in the works of literature (150 mg g⁻¹ [41], 365 mg g⁻¹ [22]). The enhanced adsorption ability can effectively improve the concentration of organic pollutants near the surface of the catalyst, thus improve the catalytic activity [39]. As the high adsorption capacity was obtained, the high catalytic performance is highly desirable.

3.3. Catalytic properties

The catalytic capacity of the prepared SMT/MoS₂ microsphere was evaluated through the color variation of organic dyes suffering from the catalytic reduction under NaBH₄. The peaks of MB and 4-NP, with the initial peak at 665 nm and 400 nm, respectively, were decreased with the prolonging catalytic reduction time. The process can be easily monitored by UV-vis spectroscopy. As shown in Fig. 5a and 5b, the absorbance peak decreases rapidly within 7 min and 6 min, respectively. The catalytic reduction process is not only eliminated the visual pollution but also alter the carcinogenicity to low and no bioactivity [34]. For example, upon the catalytic reduction process, the color of the

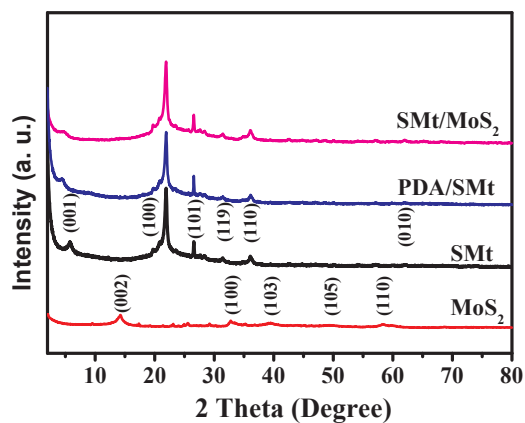


Fig. 2. XRD patterns of SMt, MoS₂, PDA/SMt, and SMt/MoS₂.

MB solution changed from blue to almost colorless, accordingly, the carcinogenic MB was altered to inactive form leucomethylene blue (LMB) [35]. Furthermore, reaction kinetics were investigated. As shown in Fig. 5c, both the catalytic processes of samples exhibit the linear relationships, demonstrating the pseudo-first-order reaction kinetics. From the linear relation of $\ln(C_t/C_0)$ with the reaction time, the apparent reduction rate constant (K) was obtained. The values of K were 0.381 min⁻¹ and 0.307 min⁻¹ for MB and 4-NP, respectively. The catalytic mechanism of SMt/MoS₂ microsphere is based on the electron transfer from the electron donor to the electron acceptor [35]. The catalytic activity is mainly related to the surface area providing for electron transfer. Thus, the optimized K can be obtained through tailoring the concentration of catalyst. As shown in Fig. 5d, the K values can increase linearly to 0.755 min⁻¹ with the concentration of SMt/MoS₂ microsphere increasing from 200 mg L⁻¹ to 1000 mg L⁻¹ and unaltered concentration of 4-NP and NaBH₄ (250 mg L⁻¹ and 0.5 M, respectively). The K towards 4-NP is much higher than the MoS₂ (0.235 min⁻¹) and Mt/MoS₂ (0.874 min⁻¹ and 0.723 min⁻¹) reported in the literature due to the good dispersion of MoS₂ nanosheets and high adsorption of SMt substrates towards organic dyes [30,31].

3.4. Recyclability examination

Considered the cost of MoS₂ and water containing organic pollutants, recyclability is the most promising approach for the application of the prepared SMt/MoS₂ microsphere. In this work, successive 20 cycles were applied to evaluate the recyclability of prepared catalysts. As shown in Fig. 6a and b, SMt/MoS₂ exhibits excellent catalytic stability achieving almost 100% efficiency in the 15 cycles and slightly decreasing less than 1.5% in the 20 cycles. Furthermore, as shown in Fig. 6c and d, the catalytic performance is almost unaltered upon 20 cycles. The K decreased by less than 5%. The mass loss percent of SMt/MoS₂ microsphere after recovery was weighted. After the centrifugation process, the values of the microspheres after 1, 5, 10, and 20 cycles for catalytic reduction of MB were decreased by 98.5 wt%, 97.2 wt%, 96.4 wt%, and 95.5 wt%, well agreeing with the decreased ratio of K. Thus, the slightly decreased K after recyclability experiment can be attributed to the mass loss of catalyst. Furthermore, as shown in Fig. 6e and f, the morphology of the prepared SMt/MoS₂ microsphere was almost unchanged after 20 cycles. In addition, as shown in Fig. S6, the XRD pattern of SMt/MoS₂ microsphere after catalytic cycle 20 times was almost unaltered. All their results reflect the excellent stability of the prepared microsphere.

4. Conclusions

The micro-sized granular SMt/MoS₂ microsphere was facile fabricated through the polydopamine method. MoS₂ nanosheets stably fixed on the surface of porous SMt, effectively solving the aggregation problem and further providing the abundant active sites. Besides, the prepared microsphere can effectively adsorb the organic pollutants due to its porous structure, thus, improved the concentration of organic pollutants near the surface of catalysts. These advantages validly facilitate the catalytic performance of organic pollutants. Furthermore, the prepared SMt/MoS₂ microsphere can be easily recovered from the mixture without any device involved due to the self-sedimentary property. After recycling 20 times, the morphology of SMt/MoS₂ microsphere still keep stable and the catalytic reduction efficiency was almost unaltered. Our straightforward approach to solving the

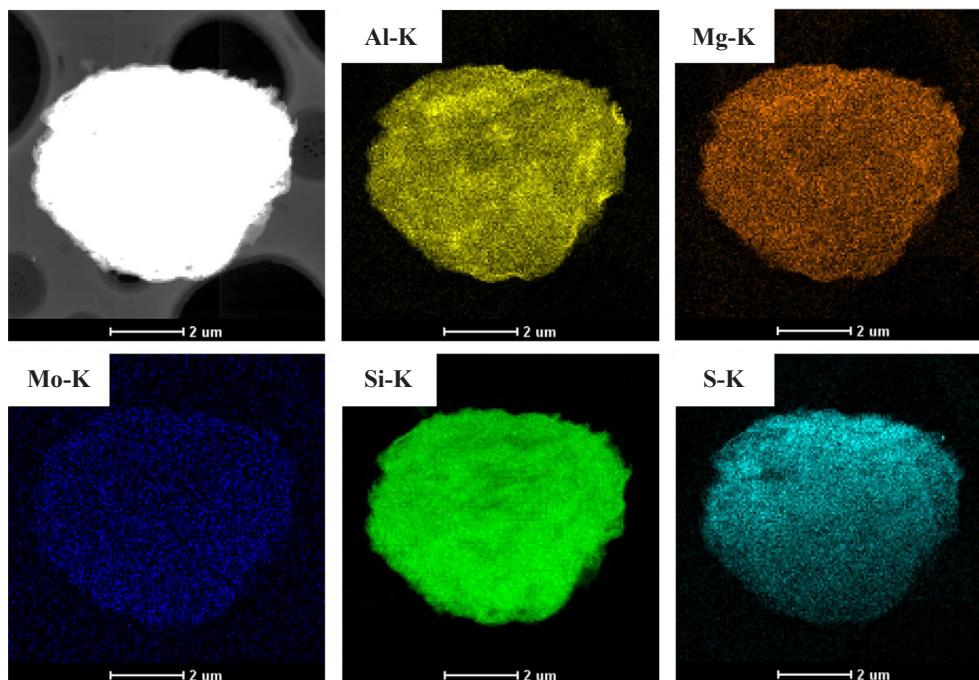


Fig. 3. HAADF-STEM image and the corresponding STEM-EDX elemental mapping images of the SMt/MoS₂ microspheres.

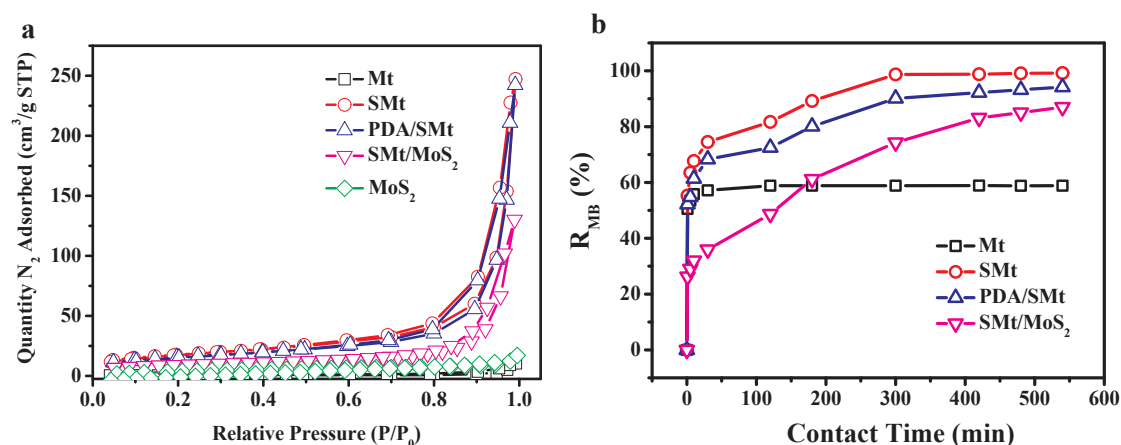


Fig. 4. The N_2 adsorption (a) and adsorption kinetics of model organic pollutant MB (b) on the Mt, SMt, PDA/SMt, and SMt/MoS₂ microspheres.

Table 1

Mesoscale properties of Mt, SMt, PDA/SMt, SMt@MoS₂, and MoS₂.

Sample	BET surface area ($m^2 g^{-1}$)	Pore volume ($cm^3 g^{-1}$)
Mt	8.2	0.10
SMt	60.6	0.38
PDA/SMt	45.6	0.24
SMt@MoS ₂	31.3	0.20
MoS ₂	16.0	0.03

problems of aggregation and recyclability through self-sedimentary micro-sized porous granular nanomaterials as the substrate may pave a promising way to produce high-performance catalyst for application.

Author contributions

All authors have given approval to the final version of the manuscript.

CRediT authorship contribution statement

Hongzhen Wang: Writing - original draft. Ning Wang: Writing -

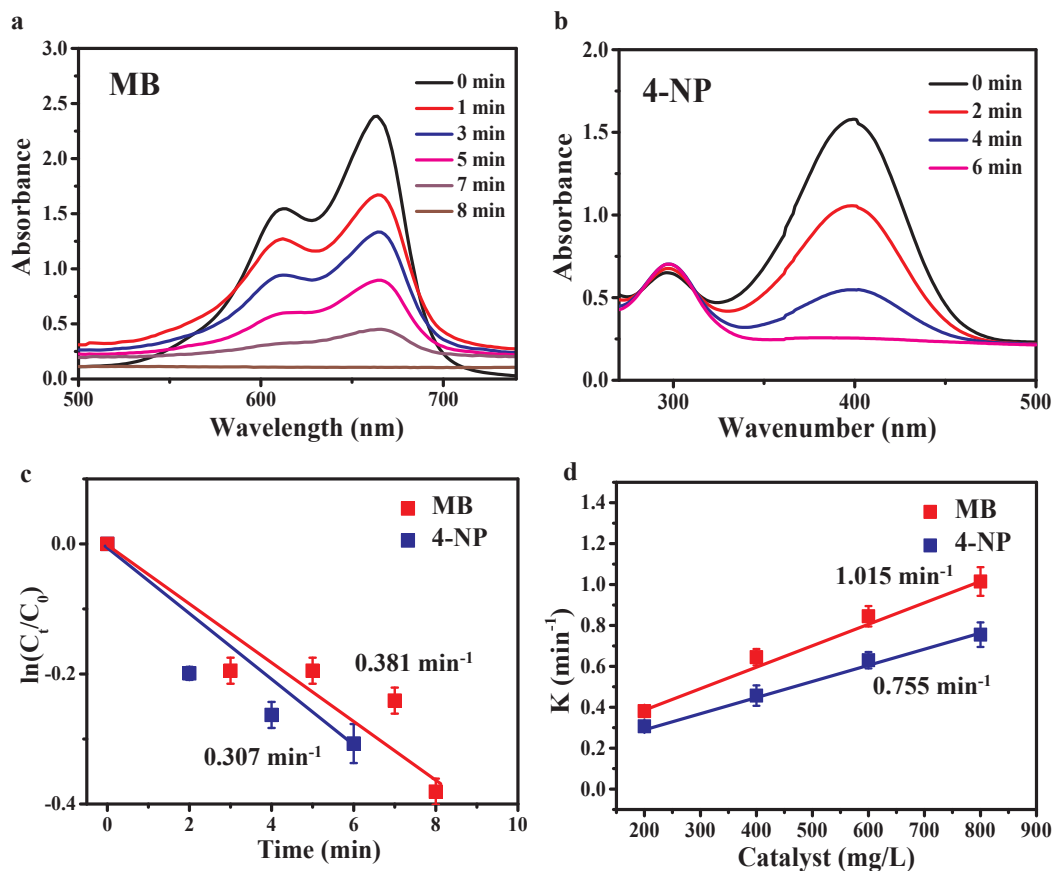


Fig. 5. Time-resolved UV-Vis spectra of MB (a) and 4-NP (b) solutions. Plot of $\ln(C_t/C_0)$ versus reaction time for the catalytic reduction of MB and 4-NP (c). The apparent reduction rate constant (K) of MB and 4-NP varies as a function of the concentration of microspheres (d).

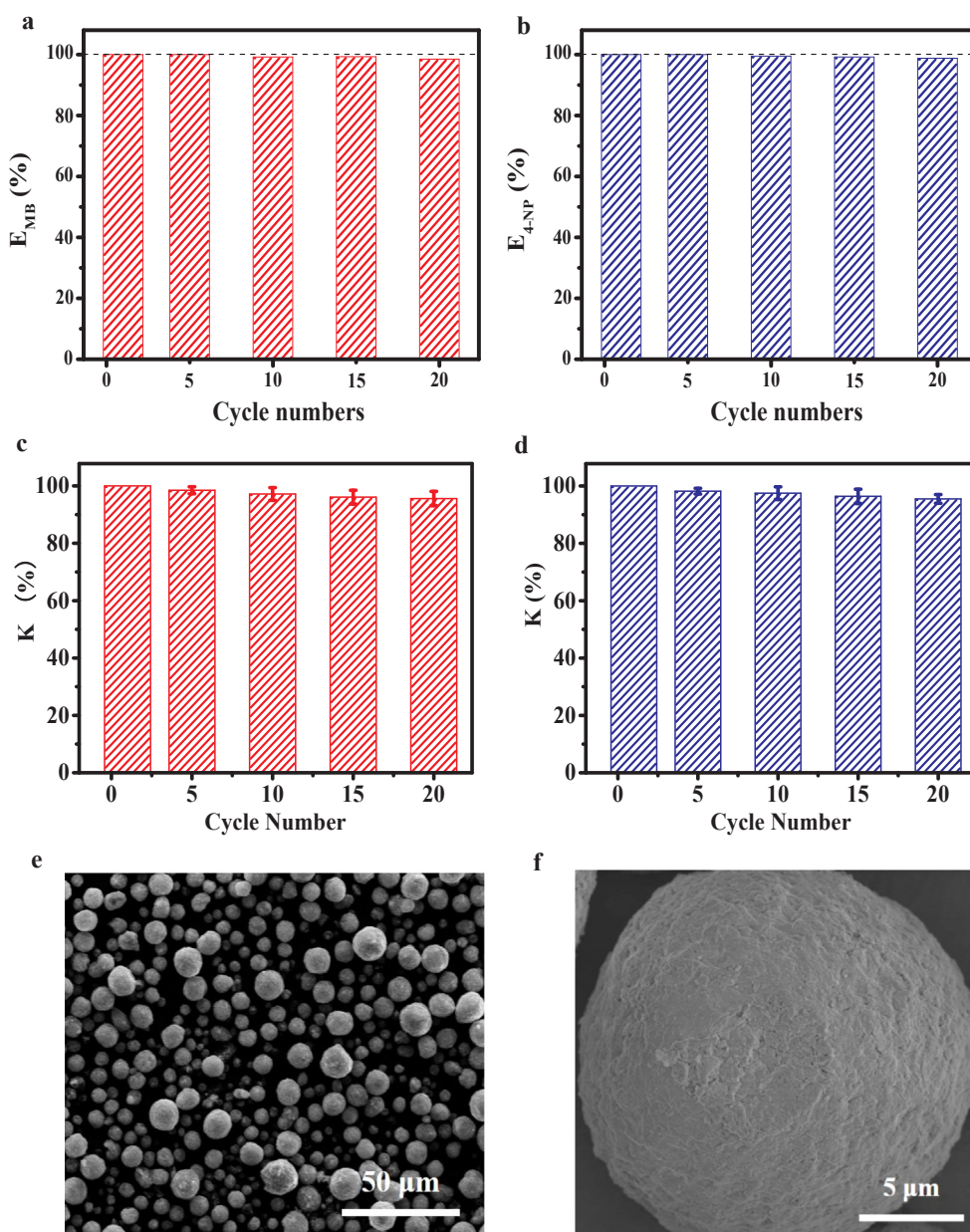


Fig. 6. The changes of apparent reduction rate constants K of microspheres in the reduction of MB (a) and 4-NP (b) with the prolonged cycle number. SEM images of SMT/MoS₂ microspheres after 20 cycles for MB (c) and 4-NP (d), respectively.

review & editing. **Fushuai Wang:** Writing - original draft. **Fengyan Xiao:** Writing - original draft. **Dawei Pan:** Writing - review & editing.

Declaration of Competing Interest

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

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Appendix A. Supplementary material

Supplementary data to this article can be found online at <https://doi.org/10.1016/j.seppur.2020.117346>.

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