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In-situ kinetic and thermodynamic study of 2,4-dichlorophenoxyacetic acid adsorption on molecularly imprinted polymer based solid-phase microextraction coatings



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ARTICLE INFO

Article history: Received 2 April 2020 Received in revised form 30 June 2020 Accepted 30 June 2020 Available online 17 July 2020

Keywords: Adsorption kinetics Adsorption thermodynamics 2,4-Dichlorophenoxyacetic acid Molecularly imprinted polymer SPME coating Fiber-optic sensing

ABSTRACT

Solid-phase microextraction (SPME) is attracting increasing interest due to being promising, new and green sample-preparation technique. Despite the vast research on the SPME, little is known about adsorption kinetics and thermodynamics of SPME coating, which plays the key role in the extraction. In this paper, a blade type SPME coating was prepared on glass slide, and 2,4-dichlorophenoxyacetic acid (2,4-D) adsorption on the coating were monitored by in-situ fiber-optic sensing. The effects of contact time, temperature (298-318 K) and initial concentration (20-150 mg/L) of 2,4-D on the adsorption properties of SPME coating were discussed. The results demonstrated that the pseudo-second-order model was most suitable for describing 2,4-D adsorption on the SPME coating. The thermodynamic parameters (ΔH , ΔS , ΔG) indicate that 2,4-D adsorption at low concentration by the SPME coating is exothermic and spontaneous process. Under the same conditions, the molecularly imprinted polymers (MIPs) coating have significantly higher adsorption capacity, and faster adsorption rate than the non-imprinted polymers (NIPs) SPME coating. This approach provides a tool for in-situ monitoring of adsorption kinetics and thermodynamics of SPME coating which requires fast measurement and small volume.

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1. Introduction

2,4-dichlorophenoxyacetic acid (2,4-D) is used as a herbicide and plant growth regulator in agriculture, such as in rice and wheat due to its low-cost [1,2]. However, 2,4-D has been testified to be toxic to human body, according to the World Health Organization (WHO). The maximum concentration of 2,4-D in drinking water should not more than 70 μ g/L [3,4]. In addition, 2,4-D has been detected in water bodies all over the world and found to be hardly degradable.

At present, 2,4-D has been determined mainly by high performance liquid chromatography (HPLC), immunoassays [5], gas chromatography (GC) [6], gas chromatography-mass spectrometry (GC-MS) [7], and liquid chromatography-mass spectrometry

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https://doi.org/10.1016/j.sna.2020.112190 0924-4247/© 2020 Elsevier B.V. All rights reserved.

(LC-MS) [8]. The sample matrix is often very complex, and the 2,4-D concentration is very low. It is usually necessary to separate and enrich the low concentration of 2,4-D in the samples. Solid-phase microextraction (SPME) has been applied increasingly for sample preparation due to its easy miniaturization, automation of devices, and its convenience in coupling with chromatographic instruments [9-11]. Ideally, SPME coatings possess high adsorption capacity, selectivity and fast kinetics, as well as high stability. Commercial SPME coatings include polyacrylate (PA), polydimethylsiloxane (PDMS), divinylbenzene (DVB), carbowax/divinylbenzene (CW/DVB), divinylbenzene/carboxen/polydimethylsiloxane (DVB/CAR/PDMS) and carboxen (CAR) [12]. However, these are common coatings used for a broad range of analytes with different polarity, almost without any specificity. And they also suffer from poor stability due to physical attachment on the substrate [13,14]. Chemical immobilization can be a good alternative to address this limitation. Polymer coatings prepared by sandwich method have good physical robustness,

controllable thickness, thermal stability and reusability. Molecularly imprinted polymers (MIPs) is a kind of material for selective recognition of target molecules [15–17], and have been widely used in sample pretreatment due to their high selectivity and low cost [18,19]. Although extensive research has been carried out on SPME coating materials, there are few studies that have systematically investigated their adsorption characteristics.

Fiber-optic sensing technology has been increasingly used in the fields of energy, environmental protection, industrial control, medicine and health and construction [20,21]. Fiber-optic sensor has the advantages of being in-situ, real-time and fast response [22]. Compared with the traditional manual sampling method, the fiberoptic sensing in-situ detection method is labor-saving, simple and highly accurate. The traditional manual sampling method can cause the solution loss and affect the measurement accuracy. The in-situ fiber-optic detection method can address all of these problems.

In this study, a blade type SPME coating was successfully prepared on the glass slides via covalent bonding using molecular imprinting techniques. In-situ fiber-optic sensing was presented for continuously real-time monitoring of 2,4-D adsorption process on the MIPs and NIPs coatings.

2. Materials and methods

2.1. Materials

Ethylene glycol dimethacrylate (EGDMA), 2,2-azobis isobutyronitrile (AIBN), 3-(Methacryloyloxy) propyltrimethoxysilane (MPS) and 2,4-dichlorophenoxyacetic acid (2,4-D), 2,4dichlorophenylacetic acid (DPAc), 4-chloroxyphenylacetic acid (CPOAc) and 4-chlorphenylacetic acid (CPAc) were purchased from the Tokyo Chemical Industry Co. Ltd. (Shanghai, China). Analytical grade methanol and ethanol were obtained from Sinopharm Chemical Reagent Co., Ltd. (Shanghai, China). 4-vinyl pyridine (4-VP) was purchased from J&K Chemicals (Beijing, China). Polytetrafluoroethylene (PTFE) microporous membranes were obtained from Shanghai Xingya Purifying Material Factory (Shanghai, China). Glass sides were obtained from Zhejiang Yixing Glass Instrument Factory (Zhejiang, China). Ultrapure water was obtained from a purification system (Chengdu, China).

2.2. Instrumentation

The absorption spectrum was gained with an in-situ fiber-optic sensing detection system (Ocean Optics, Dunedin, Florida, USA). The system consists of a stable and continuous source of spectrum light (195-644 nm) which was provided by a DH-2000 deuterium tungsten halogen source. An HR2000 charge-coupled device spectrophotometer was connected to the light source by a fiber-optic dipping probe. The probe includes an Al-coated mirror, an illumination fiber, and all mounted in stainless steel cylinders. An adsorption vessel was assembled from a conical flask, a heating magnetic stirrer, an adsorption bag, and a fiber-optic probe. The heating magnetic stirrer was obtained from IKA (Germany). The ultrasonic cleaner was obtained from Kunshan City Ultrasonic Instrument Co. Ltd. (KQ5200E, Kunshan, China).

2.3. Polymer coating preparation

The polymer coating was prepared through a novel sandwich method with modified glass slide as substrate and a microporous membrane as support material. The detailed preparation process of polymer coating was described in the supplementary materials. Fig. A.1 shows a schematic illustration of the preparation of the polymer coating.

3. Experimental method

3.1. Stock solution

Preparation of 2,4-D 500 mg/L stock solution was accomplished by accurately weighting of standard sample and completely dissolving in methanol, and then the volume was fixed with ultrapure water. The stock solution was stored in a refrigerator for later use.

3.2. Calibration curve

The stock solution was diluted with methanol-water (v/v, 1:9) to obtain a series of 2,4-D calibration solutions in the range of 5-200 mg/L. The different concentrations of 2,4-D solution were detected by the in-situ fiber-optic spectrophotometer at 283 nm according to the following procedure:

(1) The deuterium lamp of the fiber-optic light source was opened and preheated for 30 min;

(2) The spectra suite software was turned on, fiber-optic probe was immersed into solvent (as reference) and bubbles in probe window were removed;

(3) The integration time and smoothing width were adjusted to 24 ms and 5, respectively. The light intensity level was adjusted around 3200 counts at the 283 nm (detection wavelength), and the signal intensity, reference and dark spectra were stored;

(4) The fiber-optic probe with light-path of 5 mm was immersed into the vessels containing 3 mL of 2,4-D solution with different concentrations, respectively. Then, obtain the absorbance of each 2,4-D solution was obtained.

The same system configuration described above was used in the rest of the work.

3.3. Batch experiments

Four pieces of SPME coatings were placed in a vial and soaked in methanol-water (v/v, 1:9) for 1 h to activate the coatings. The fiberoptic probe was dipped in 2,4-D solution of different concentrations and the instrument parameters were adjusted. The activated four pieces of SPME coatings were put into the adsorption solution as shown in picture Fig. A.2, and the adsorption was carried out at 200 rpm and 298 K. If the absorbance of adsorbate does not change more than 0.002 within 30 min, it was considered that the process reached adsorption apparent equilibrium stage. Finally, the light source was turned off and stored the experimental data. Through the above experimental method, the adsorption behavior of 2,4-D with different concentrations (20-150 mg/L) on SPME coatings was monitored at 298-318 K. The adsorption isotherm was obtained by using the relative equilibrium concentration $C_{\rm e}$ (mg/L) as abscissa and the adsorption capacity $Q_{\rm e}$ (mg/g) as ordinate. The adsorption and desorption capacity of 2,4-D were calculated by the following equations:

$$Q_e = \frac{(C_0 - C_e)}{m} V_i \tag{1}$$

$$D_e = \frac{C_d}{m} V_d \tag{2}$$

where C_0 and C_e are the initial and the relative equilibrium concentrations of the sample solutions (mg/L); V_i indicates the total volume of the sample solution used in the study (L); C_d and V_d are the concentration (mg/L) and volume (L) of the desorption solution of 2,4-D. m is the weight of the polymer (g); Q_e stands for the adsorption capacity at adsorption equilibrium (mg/g); D_e is the desorption capacity when desorption reaches relative equilibrium (mg/g).

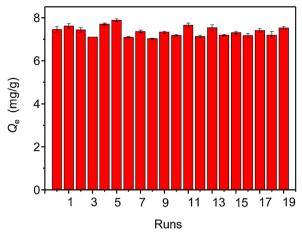


Fig. 1. Reusability of MIPs coating.

4. Results and discussion

4.1. Stirring speed

In order to investigate the effect of stirring speed on adsorption capacity of the SPME coating, the magnetic stirring speeds of 100, 200 and 300 rpm were selected to investigate the effect of stirring speed on the adsorption by in-situ measurement. Fig. A.4 provides an overview in the time of 250 min, with the increasing of agitation speed, the adsorption capacity increases, which may be due to good stirring makes the solution distribute more uniformly [23]. When the stirring speed increases from 200 rpm to 300 rpm, the adsorption capacity of SPME coating changes little. However, the surface of the SPME coatings will be destroyed if the mixing speed is too fast, and it is also a challenge to the fixing of the SPME coatings in the vial. Therefore, 200 rpm was selected for rest of the study.

4.2. Regeneration performance of SPME coating

To be an effective SPME device, the regeneration and reuse of SPME coating are essential. Under the same conditions, adsorptiondesorption experiments were repeated on the fiber-optic sensing detection system. As shown in Fig. A.5, the relative standard deviation (RSD) value of adsorption capacity at the same time point of three groups of parallel experiments was 1.78 %. In this study, the MIPs coatings were regenerated by extraction using 10 % acetic acid-methanol. In addition, as shown in Fig. 1, the adsorption capacity of MIPs did not change significantly after 19 runs (RSD less than 3.2 %), indicating that MIPs coatings have good regeneration ability and can be used as a good SPME material for the separation and enrichment of trace 2,4-D in environmental samples.

4.3. Adsorption kinetics

4.3.1. Adsorption kinetic curves

The adsorption kinetic curves of 2,4-D on different SPME coatings obtained by the system at 298 K are shown in Fig. 2 (a) and Fig. A.6. With the increasing of 2,4-D concentration, the mass transfer enhances, then the SPME coating adsorption capacity increases gradually, and the relative adsorption equilibrium time gets longer. The adsorption capacity rapidly increases in the initial 40 min. In the beginning of the adsorption, interaction opportunity between solute and solvent is the largest, which makes the adsorption rate is the fastest in this stage. With the extension of adsorption time, the adsorption rate decreases and desorption rate increases. As detailed in Fig. 2 (b), under the same conditions, adsorption capacity of MIPs coating is higher than that of NIPs coating for 2,4-D. That is due to the contribution of imprinted binding sites, which was formed during the polymerization around template and the binding sites have complementary shape and size with 2,4-D molecules [24]. 2,4-D and its analogues DPAc, CPOAc and CPAc were used to investigate the selective adsorption of SPME coating. As shown in Fig. 2 (c), both MIPs and NIPs adsorbed 2,4-D and its structural analogues, but the adsorption capacity was different. It was observed that MIPs coating had the greatest binding capacity to 2,4-D compared with its analogues. This is due to MIPs has high specificity and selectivity to 2,4-D resulted from a remarkable imprinting effect.

4.3.2. Adsorption kinetic models

Adsorption rate is one of the main focuses of adsorption kinetics, which plays an extremely significant role in the whole adsorption process [25]. The adsorption process is clearly described by three kinds of kinetic models, and the equations of these kinetic models were as follows.

Pseudo-first-order model [26]:

$$ln(Q_e - Q_t) = lnQ_e - K_1 t \tag{3}$$

Pseudo-second-order model [27]:

$$\frac{t}{Q_t} = \frac{1}{K_2 Q_e^2} + \frac{t}{Q_e}$$
(4)

Intra-particle diffusion model [28]:

$$t_{1/2} = \frac{1}{K_3 Q_e} + C \tag{5}$$

where Q_e and Q_t are the adsorption capacities (mg/g) at equilibrium and at a time t, respectively. K₁, K₂ and K₃ are pseudo-first-order rate constant (1/min), pseudo-second-order rate constant (g/(mg·min) and intra-particle diffusion rate constant (mg/(mL·min^{1/2})), $t_{1/2}$ is the time required to complete half of the adsorption, C is the intra-particle diffusionmodel constant.

The fitting curves of pseudo-first-order and pseudo-secondorder models of 2,4-D adsorption on NIPs and MIPs coatings are shown in Fig. 3 (a) and (b). The parameters of the two models are listed in Table 1. Table 1 shows that the R^2 values ($R_{NIPs}^2 = 0.8943$, $R_{MIPs}^2 = 0.9635$) of pseudo-first-order model was smaller than that of pseudo-second-order model ($R_{NIPs}^2 = 0.9927$, $R_{MIPs}^2 = 0.9983$). In addition, under different initial concentration conditions (C_0) , the theoretical value of equilibrium adsorption capacity (Q_{cal}) calculated by the pseudo-first-order model was considerably different from the experimental adsorption capacity (Q_{exp}) obtained from the experiments (error was 34.94-66.36 %). However, the error between the theoretical value of Q_{cal} from the pseudo-secondorder model and the Q_{exp} was less than 10 %. High correlation coefficient and low error values indicate that the pseudo-secondorder model can more accurately describe the adsorption behavior of 2,4-D on MIPs and NIPs coatings [29].

The adsorption kinetics of 2,4-D on MIPs and NIPs coatings are controlled by the adsorption mechanism and intra-particle diffusion rate. As identified from Fig. 3 (c), the plots of Q_e versus $t_{1/2}$ don't give straight line within whole adsorption process, but represent a multicollinearity, which indicates that two or more stages exist in the adsorption of 2,4-D on MIPs. It can be explained that adsorption process is carried out in three consecutive steps [30]: (1) Instantaneous adsorption of adsorbate on the surface of adsorbent, (2) diffusion of adsorbate molecules in adsorbent pores, (3) adsorption of adsorbate molecules on the inner surface of the adsorbent. Adsorption of 2,4-D on MIPs and NIPs coatings can be divided into three stages, none of the three fitted lines can pass through the origin point of the coordinate. This indicates that the intra-particle diffusion is not the only speed limiting step, and the process can also be controlled by external mass transfer and internal diffusion

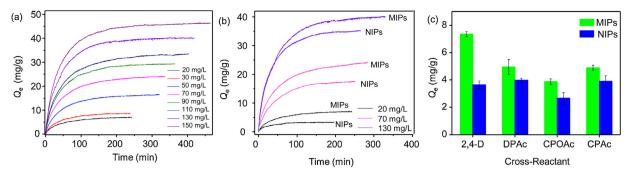


Fig. 2. Adsorption kinetic curves of 2,4-D on different SPME coatings at 298 K (a) MIPs (b) MIPs and NIPs (c)Selectivity adsorption of SPME coating of MIPs and NIPs.

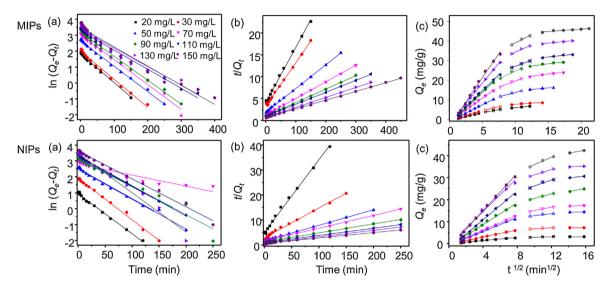


Fig. 3. Fitting plots of adsorption kinetic models to 2,4-D on SPME coatings (a) pseudo-first-order (b) pseudo-second-order (c) Intra-particle diffusion.

 Table 1

 Kinetic parameters of pseudo-first-order and pseudo-second-order models for 2,4-D on NIPs and MIPs SPME coatings.^a

Adsorbent	$C_0 (mg/L)$	$Q_{\exp} (mg/g)$	Pseudo-first-order Q _{cal} (mg/g)	K ₁ ×10 ² (1/min)	R ²	Pseudo-second-order Q _{cal} (mg/g)	$K_2 \times 10^4 (g/(mg \cdot min))$	R ²
	20	7.02	4.14	1.79	0.9931	7.56	37.8627	0.9977
	30	8.73	4.70	1.75	0.9897	9.11	29.4021	0.9983
	50	16.43	7.81	1.58	0.9958	18.08	16.0191	0.9991
MID	70	23.98	10.63	1.56	0.9888	26.25	12.1230	0.9987
MIPs	90	29.42	11.81	1.5	0.9934	32.57	9.5182	0.9998
	110	33.53	12.58	1.19	0.9864	36.36	8.0926	0.9996
	130	40.81	13.73	1.16	0.9635	43.86	7.7139	0.9994
	150	46.37	14.92	1.2	0.968	49.75	6.7696	0.9996
	20	3.18	2.07	2.51	0.9944	3.43	171.0975	0.9950
	30	7.42	4.42	2.59	0.9963	7.39	50.6258	0.9927
	50	14.57	7.01	1.89	0.9916	16.16	23.2543	0.9989
	70	21.47	8.85	0.69	0.8943	19.61	16.6358	0.9938
NIPs	90	25.04	11.57	1.76	0.9510	27.70	11.2725	0.9976
	110	30.61	13.01	1.88	0.9976	33.72	9.0442	0.9989
	130	34.98	14.85	2.47	0.9764	38.46	11.8972	0.9990
	150	42.63	16.86	1.75	0.9929	46.29	6.9100	0.9974

^a Q_{exp} and Q_{cal}, apparent and calculated equilibrium adsorption capacity, respectively; K₁, pseudo-first-order rate constant; K₂, pseudo-second-order rate constant; R², correlation coefficient.

of particles. The values of K_{id1} , K_{id2} , K_{id3} , and C_1 , C_2 , C_3 in the adsorption process are summarized in Table A.1. According to Fig. 3 (c) and table A.1, the adsorption rates of 2,4-D on MIPs and NIPs coatings are obviously different. In the first and second step, the adsorption of 2,4-D on the MIPs coatings is faster. In the third step, the low free concentration of 2,4-D and the very limited adsorption sites of coating result in a relative equilibrium. However, the adsorption on the MIPs coatings is still growing. Great number of recognition sites of MIPs coatings are attributed to higher specific adsorption capac-

ity against 2,4-D. The main specific interactions of the MIPs SPME coating are resulted from ionic bonds and hydrophobic interactions [31].

4.4. Adsorption thermodynamics

An adsorption isotherm is a method to measure the relationship between the equilibrium concentrations and adsorption capacity when adsorption reaches dynamic equilibrium in a certain concen-

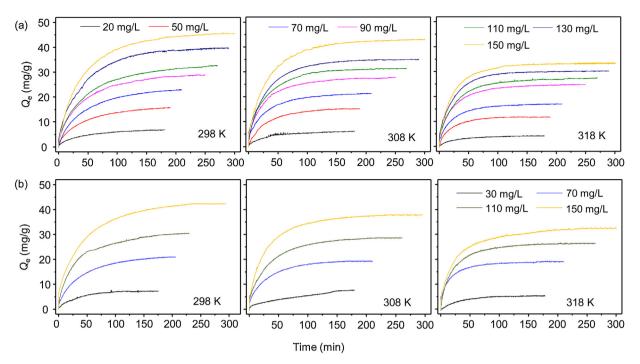


Fig. 4. Adsorption kinetics of 2,4-D on polymer coatings at different temperatures (a) MIPs (b) NIPs.

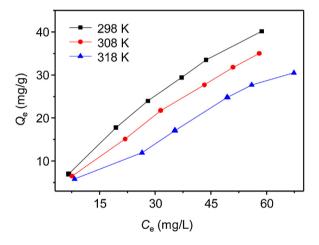


Fig. 5. Adsorption isotherms of 2,4-D on MIPs SPME coatings.

tration range [32]. At 298, 308 and 318 K, the adsorption process of 2,4-D on SPME coatings were monitored by in-situ fiber-optical spectrometer, and the adsorption capacity was calculated according to equation (1). The adsorption kinetics of MIPs and NIPs coatings for 2,4-D at different temperatures are illustrated in Fig. 4. The adsorption isotherms were obtained using the equilibrium concentration as horizontal coordinate and adsorption amount as vertical coordinate (Fig. 5). The adsorption capacity of 2,4-D increases with the increasing of concentration. With the increasing of temperature, the adsorption capacity of the MIPs coating decreases. Generally, low temperature is favorable for the adsorption.

Langmuir model is an adsorption isotherm model based on the basis of kinetics viewpoint. This theory has assumptions that [33] (1) the adsorption takes place on the monolayer of the adsorbent, and only one molecule is adsorbed at each adsorption site, (2) there is no interaction between the adsorbed molecules, (3) the enthalpy

values of all adsorbed molecules are equal. Langmuir isotherm model was determined as [34]:

$$\frac{1}{Q_e} = \frac{1}{K_L Q_{max}} \frac{1}{C_e} + \frac{1}{Q_{max}}$$
(6)

Freundlich isotherm model is one of the empirical equations for heterogeneous adsorbents. The adsorption energy of each site is different. It is assumed that (1) the adsorption heat decreases with the increase of the coverage area of the adsorbent, (2) the adsorption points on the adsorbent surface have different adsorption energies. The Freundlich equation is determined as follows:

$$lnQ = lnK_F + \frac{1}{n}lnC_e \tag{7}$$

The basic characteristics of adsorption isotherms can be expressed by the separation factor (R_L). The R_L is expressed as [35]:

$$R_L = \frac{1}{1 + K_L C_0} \tag{8}$$

In these equations, Q_e and Q_{max} are the equilibrium adsorption capacity and maximum adsorption capacity (mg/g), respectively. C_e is the concentration of solution when the adsorption reaches relative equilibrium (mg/L). K_L is the Langmuir constant (L/mg), K_F is the Freundlich constant or the value of Q_e at $C_e = 1$ mg/L (mg/g)·(L/mg)^{1/n}. n is the heterogeneous factor related to the adsorption intensity. R_L is the separation factor. $R_L = 0$, the adsorption process is irreversible. $R_L = 1$, the adsorption process is linear. If $R_L>1$, the adsorption process is unfavorable. $0 < R_L < 1$, the SPME coating is favorable for 2,4-D adsorption.

The curves of isotherm models are presented in Fig. A.7. Table 2 summarizes the isotherm parameters of 2,4-D adsorption, comparing R^2 of the two isotherm models, Langmuir model is more suitable for the isothermal adsorption data of NIPs. The results indicate that the adsorption of the NIPs coating for 2,4-D could be a single molecular layer adsorption. But the Langmuir model is better than Freundlich model in fitting 2,4-D isotherm adsorption data of MIPs at low temperature according to the values of R^2 . At the higher temperature, the Freundlich model is more suitable for isotherm adsorption data with the increase of temperature. From Table 2, it

Adsorbent	ΤK	Langmuir				Freundlich			
		$Q_{\rm max} mg/g$	K _L L/mg	R _L	R ²	$K_F(mg/g)(L/mg)^{1/n}$	1/n	R ²	
	298	36.63	0.0094	0.4149 to 0.8417	0.9273	5.9787	1.3349	0.9391	
NIPs	308	44.64	0.0075	0.4706 to 0.8696	0.9541	4.2338	1.2032	0.9397	
	318	26.16	0.0086	0.4367 to 0.8532	0.9236	9.0603	1.3326	0.9077	
	298	123.44	0.0092	0.4202 to 0.8446	0.9999	1.5543	0.8110	0.9964	
MIPs	308	86.73	0.0106	0.3861 to 0.8251	0.9966	1.1883	0.8350	0.9987	
	318	64.06	0.0120	0.3571 to 0.8065	0.9954	1.0604	0.8029	0.9983	

Langmuir and Freundlich isotherm constants of 2,4-D on SPME coatings.^b.

^b Q_{max}, maximum adsorption capacity (mg/g); C_e, concentration of solution when the adsorption reaches relative equilibrium (mg/L); K_L, Langmuir constant (L/mg); K_F, Freundlich constant; *n*, heterogeneous factor; R_L, separation factor.

Та	bl	e	3

Adsorption thermodynamic parameters of 2,4-D on SPME coatings.^c

Adsorbent	C ₀ mg/L	<i>∆H</i> kJ/mol	∆SJ/(mol·K)	∆G kJ/mol		
				298 K	308 K	318 K
	30	-4.17	-10.61	1.25	1.79	1.25
NUD	70	-7.29	-18.85	1.02	1.54	1.02
NIPs	110	-7.73	-20.47	0.95	1.41	0.95
	150	-7.29	-19.50	2.22	2.70	2.22
	20	-15.75	-52.42	-0.13	0.39	0.92
	50	-19.46	-65.99	0.21	0.86	1.52
N (ID	70	-19.96	-68.21	0.36	1.05	1.73
MIPs	90	-18.00	-62.28	0.56	1.18	1.80
	110	-17.28	-60.13	0.64	1.24	1.84
	130	-16.25	-57.64	0.93	1.50	2.08

^c ΔG , free energy (kJ/mol); ΔH , enthalpy (kJ/mol); ΔS , entropy (J/(mol·K)).

can be obtained $0 < R_L < 1$, indicating that MIPs and NIPs coating were favorable for 2,4-D adsorption. When 1/n>1, the adsorption process is not easy to occur, and vice versa. In addition, by fitting the Freundlich model curve, it can be concluded that 2,4-D adsorption on MIPs is easier than on NIPs at the same temperature.

The free energy ΔG (kJ/mol), enthalpy ΔH (kJ/mol) and entropy ΔS (J/(mol·K)) are usually used to describe the energy change in the adsorption process. The three thermodynamic constants can be calculated by the Eq. (9) and (10), and used to evaluate the adsorption process. Under different concentrations, the linear relation of ln K_d and 1/*T* was carried out, ΔH and ΔS were calculated respectively by the slope and intercept of the obtained linear equation (Fig. A.8). Then, the Eq. (10), was used to calculate ΔG .

$$lnK_d = \frac{\Delta S}{R} - \frac{\Delta H}{RT} = ln\frac{Q_e}{C_e}$$
(9)

$$\Delta G = \Delta H - \Delta ST \tag{10}$$

in the above equation, K_d is the sorption distribution coefficient, Q_e is the adsorption capacity at equilibrium (mg/g); C_e is the equilibrium concentration of the sample solutions (mg/L); R is ideal gas constant (R = 8.314]/(mol·K)); T is the absolute temperature.

The thermodynamic parameters such as ΔG , ΔH and ΔS are the main characteristics of adsorption process. Langmuir and Freundlich are the most widely used isotherm adsorption models and for calculation of thermodynamic parameters. The adsorption enthalpy (ΔH), entropy (ΔS) and free energy (ΔG) of 2,4-D on SPME coatings are given in Table 3. The negative value of ΔH indicates that the adsorption is an exothermic process, and the adsorption capacity is inversely proportional to temperature. The absolute value of ΔH is lower than 40 kJ/mol, suggesting that adsorption of 2,4-D on SPME coatings are mainly physical adsorption [36]. The negative ΔS indicates the disorder degree of the interface between the SPME coatings and 2,4-D solution decreases after adsorption. The diffusion of 2,4-D molecules from solution to SPME coating pores is limited and the degree of freedom is reduced. In addition, adsorption of the SPME coating for 2,4-D is more feasible and spontaneous at lower concentration as ΔG decreases with the

decreasing of the concentration. The value of ΔG increases with the increasing of temperature, which demonstrates that the increasing of temperature is unfavorable to the 2,4-D adsorption on the SPME coating. It can be seen from the data in Table 3 that the ΔG value of 2,4-D adsorption on the MIPs coatings is smaller than that on the NIPs coatings. That can prove that the MIPs coating can extract 2,4-D more effectively than NIPs coatings.

5. Conclusion

Solid-phase microextraction (SPME) has been applied increasingly for sample preparation due to its easy miniaturization, automation of devices, and its convenience in coupling with chromatographic instruments. Performances of SPME devices depend on the coating adsorption property. Characterization of the adsorption is challenging due to the small size, and fast adsorption kinetics using conventional methods using manual sampling. The main goal of the current study was to design an in-situ adsorption measurement system and evaluate kinetics and thermodynamics of the blade type SPME coating. The research has shown that the system is able to detect the fast adsorption process continuously in only few milliliter adsorption solutions. The pseudo-second-order model is found to be the most suitable for describing 2,4-D adsorption on SPME coating. The thermodynamic parameters (ΔH , ΔS , ΔG) indicate that 2,4-D adsorption at low concentration by the SPME coating is exothermic and spontaneous process. Under the same conditions, MIPs coatings have higher adsorption capacity, and faster adsorption rate than NIPs coating. These findings have significant implications for the understanding of adsorption mechanism of SPME coating. It is also useful for the understanding of the adsorption nature of surface imprinted polymers. However, the scope of this study is limited to only blade type SPME coating and do not include fiber or other type of coatings. In addition, further work needs to be done to explore the effect of coating thickness on the main parameters of adsorption kinetics and thermodynamics.

CRediT authorship contribution statement

Xiaoxia Yang: Data curation, Writing - original draft, Investigation. Turghun Muhammad: Conceptualization, Methodology, Supervision, Writing - review & editing. Jingjing Yang: Software. Ayzukram Yasen: Validation. Lingxin Chen: Writing - review & editing.

Declaration of Competing Interest

No conflict of interest.

Acknowledgment

This work was supported by the National Natural Science Foundation of China (21565025).

Table 2

Appendix A. Supplementary data

Supplementary material related to this article can be found, in the online version, at doi:https://doi.org/10.1016/j.sna.2020. 112190.

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